
SOUTH COAST AIR QUALITY MANAGEMENT DISTRICT RULE 1109.1 STUDY FINAL REPORT

**Fossil Energy Research Corp.
Laguna Hills, CA**

**SCAQMD Working Group Presentation
December 10, 2020**

FERCo EXPERIENCE

- **Founded in 1984**
- **Involved with SCR Technology Since Early 1980's**
- **Experience Includes:**
 - **Overall SCR system design**
 - **Cold flow modeling of SCR systems**
 - **Start-up and optimization testing**
 - **Pilot plant studies**
 - **Fundamental laboratory studies**
- **In-house Catalyst Test Facilities**

OBJECTIVES

- **Visited 5 Major Refineries**
 - **Chevron**
 - **Marathon**
 - **Phillips 66**
 - **Torrance**
 - **Valero**
- **Goal Was to Observe First Hand Facility Constraints**
 - **Meet with facility staff and tour the facilities**
 - **Discuss challenges of implementing SCR on specific refinery systems**
 - **Review drawings of on-going SCR work, suggest configuration modifications to improve performance**
- **Assess Possibility of Improvements to Existing SCR Systems to Meet the Upcoming PR 1109.1 NO_x Requirements**

OBSERVATIONS

- **All Sites Exhibited Space Limitations to Varying Degrees**
 - **Existing open space needed for maintenance work, not available for the SCR**
 - **Workarounds have included:**
 - **Vertical system orientation**
 - **Running ductwork over existing roads**
 - **Replace air heater with SCR reactor**
- **Old Sites Hold Many Unknowns**
 - **Electrical Capacity for the SCR**
 - **Pipe Rack Capacity for NH₃ transport to the SCR**
 - **Uncertainties about underground pipes, complicates digging, foundation work**
- **Existing SCR Systems Not Designed for High (>90%) Removals**

Key SCR Issues and Parameters

Catalyst Activity (K)

- How active the material is in reducing NO_x
- f (material, geometry)

Reactor Potential

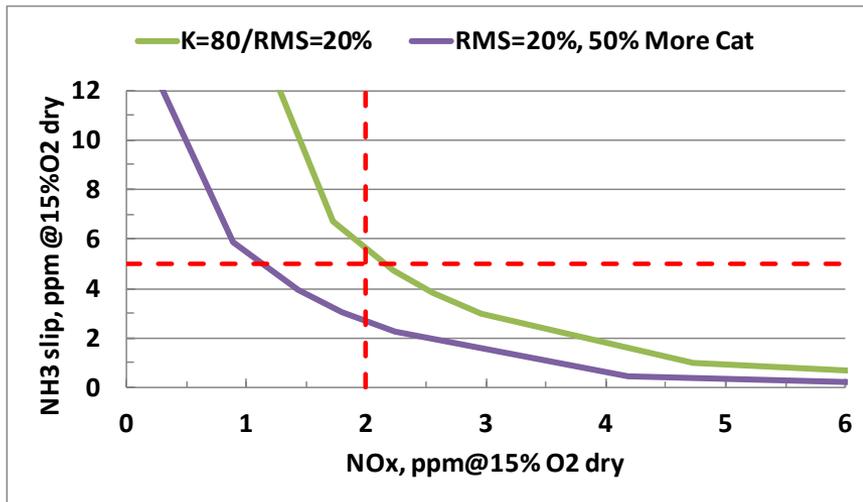
- Ability of the catalyst bed to reduce NO_x
- $\text{RP} = K \cdot A_{\text{sp}} \cdot V_{\text{cat}} / Q_{\text{fg}}$
- **Defines the Needed Catalyst Volume**
- **$\text{RP} = f(\text{NO}_{x\text{in}}, d\text{NO}_x, \text{NH}_3 \text{ slip})$**

NH_3/NO_x Distribution

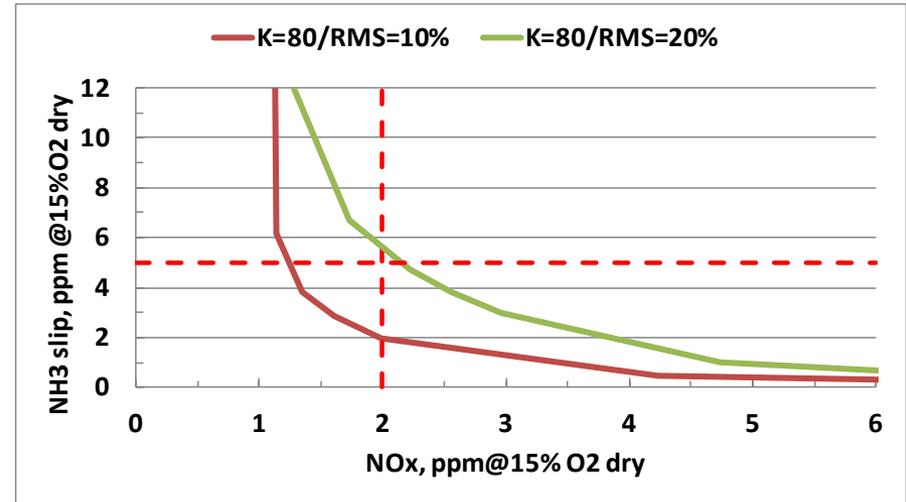
- Want NH_3/NO_x uniform across the catalyst
- Local $\text{NH}_3/\text{NO}_x > 1 = \text{NH}_3 \text{ slip}$
- **$d\text{NO}_x$ Requirement Defines NH_3/NO_x Uniformity Requirement**
- **AIG (Ammonia Injection Grid) - Mechanism by which the NH_3 is injected**
- **Characterized by RMS (STD Deviation of the NH_3/NO_x distribution entering the catalyst**
- **Higher $d\text{NO}_x$ requires lower RMS!**

How Important is the NH₃/NO_x Distribution?

RMS = 20% Add Catalyst



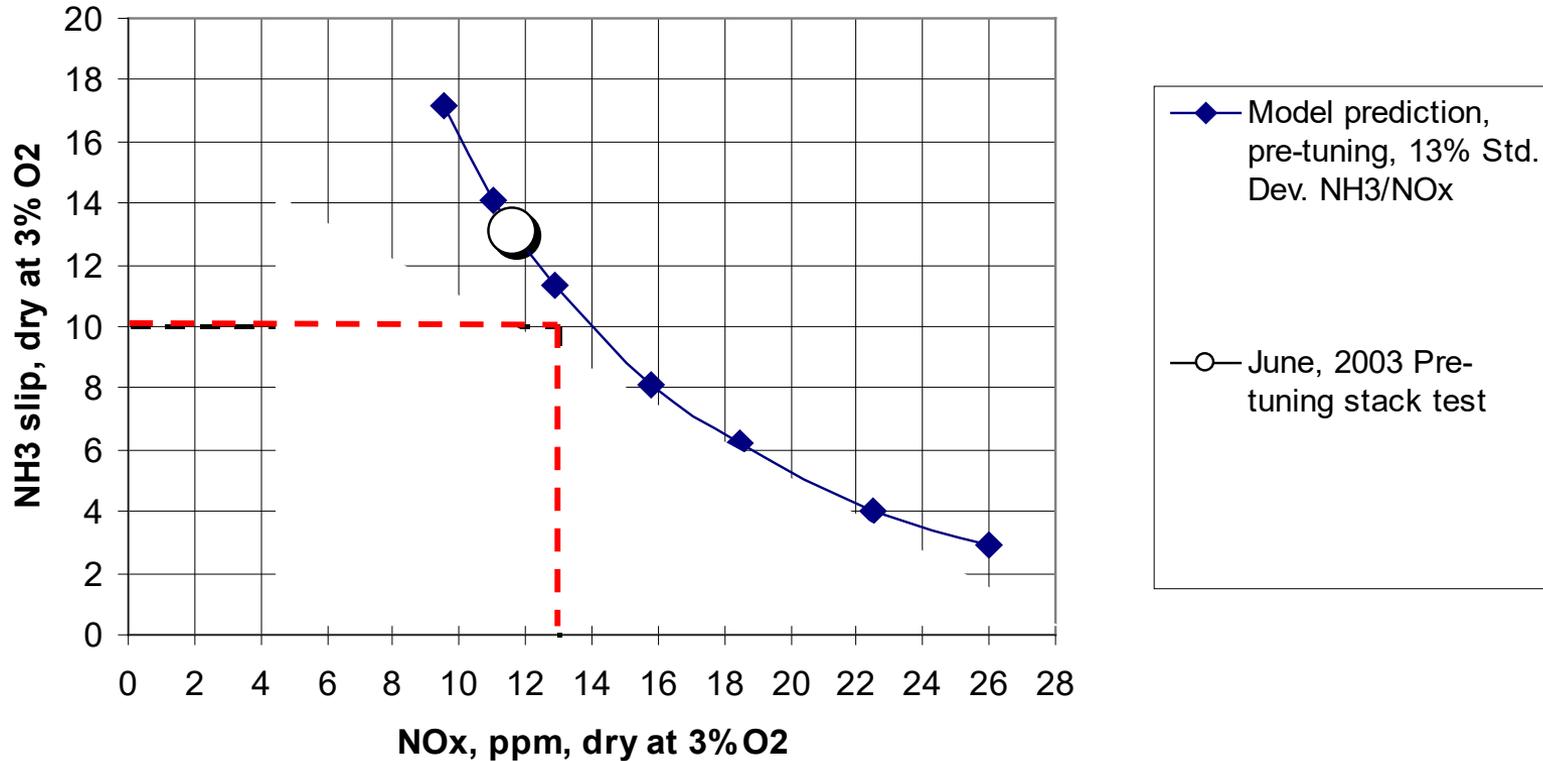
Tune AIG to RMS = 10%



- Just tuning the AIG allows 2 ppm NO_x to be achieved
- Adding 50% more catalyst helps, but not as much as tuning

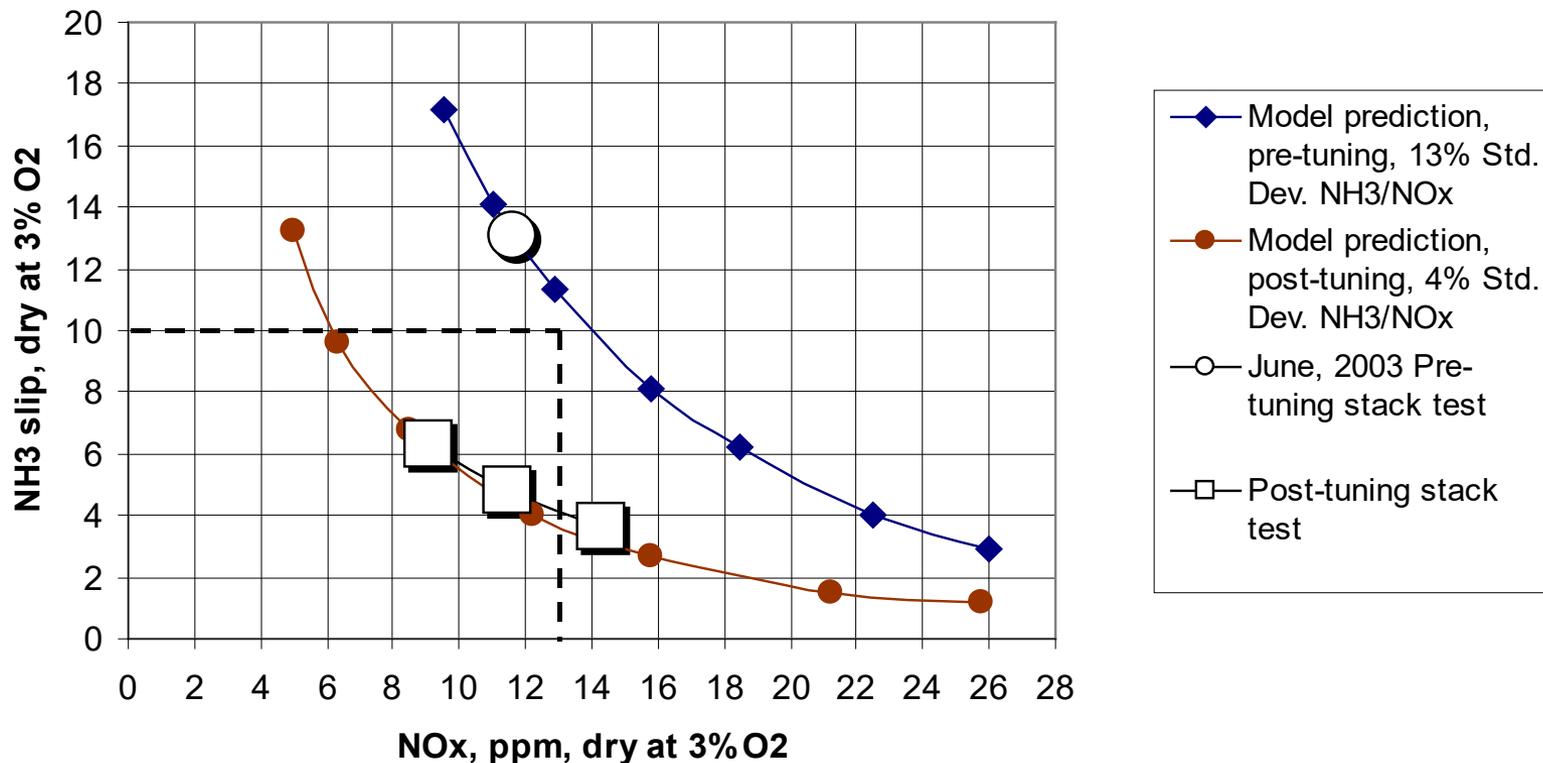
How Important is the NH₃/NO_x Distribution

AIG Tuning at South Bay 1: 141MW Boiler (2003)

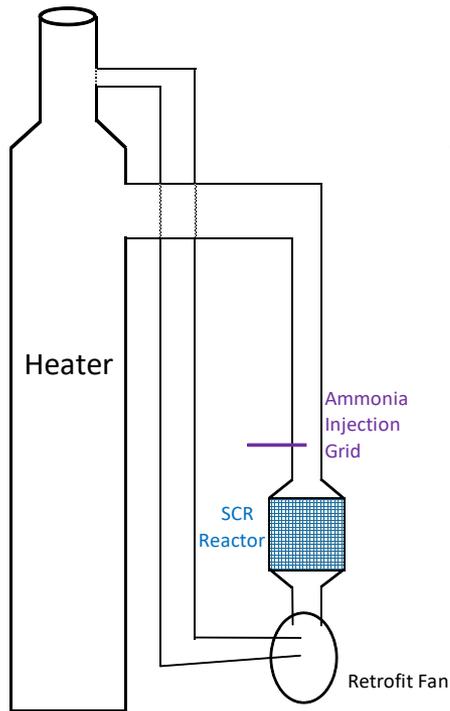


How Important is the NH₃/NO_x Distribution

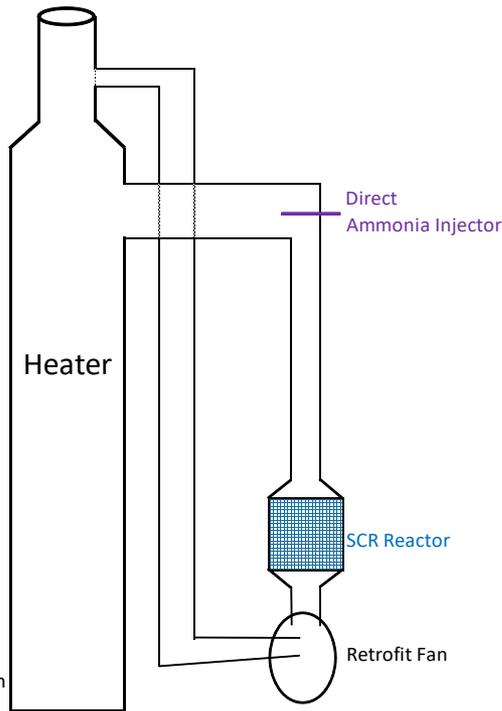
AIG Tuning at South Bay 1: 141MW Boiler (2003)



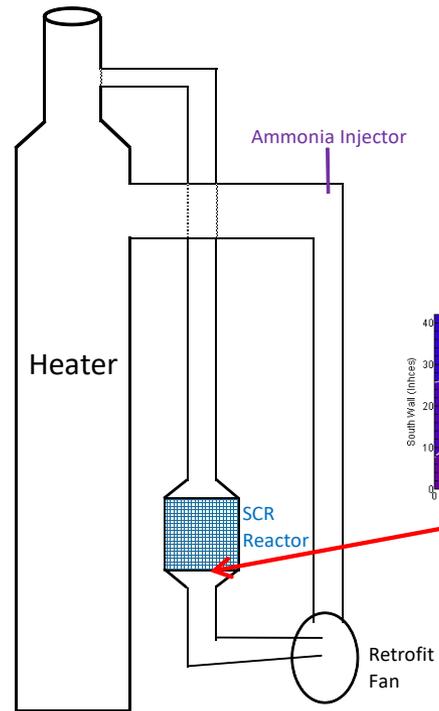
Cylindrical Heater SCR Arrangement



Traditional Arrangement

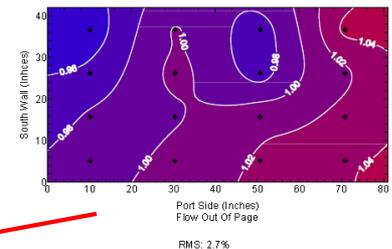


Traditional Arrangement with Direct Injection

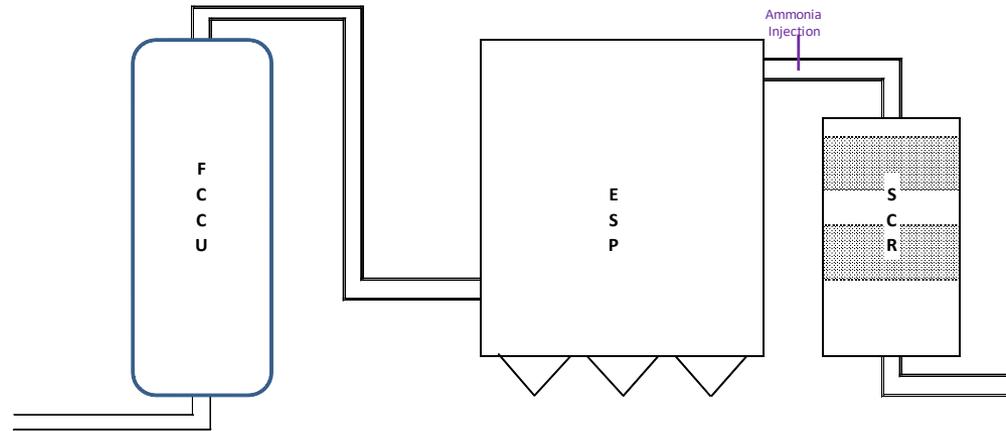


Direct Injection Using Fan as Mixing Device

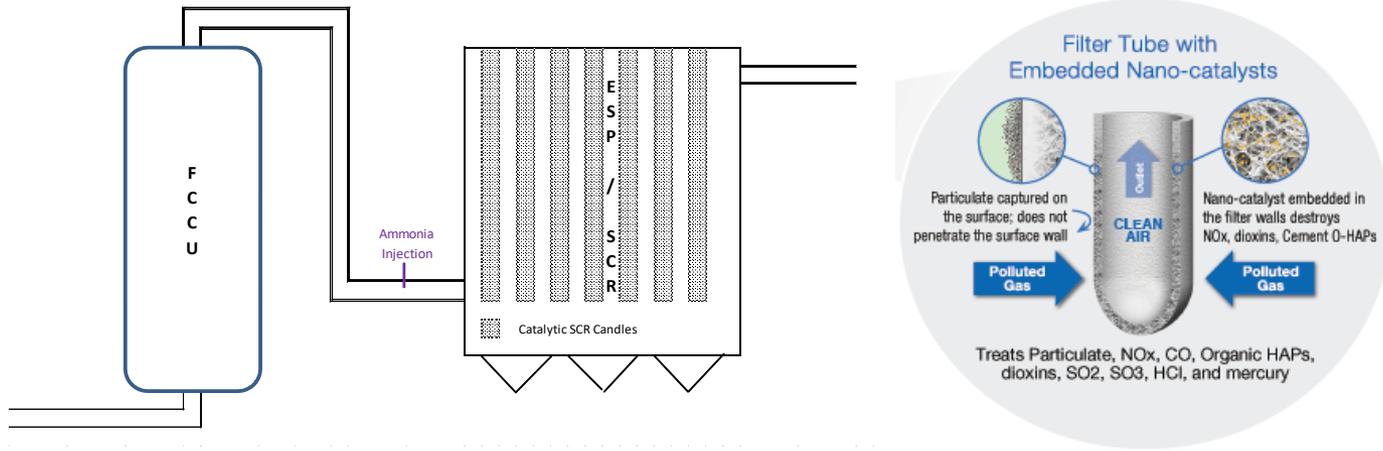
Industrial Boiler S.Cal w/ NH₃ inj. ahead of fan; RMS=2.7%



FCCU NO_x CONTROL OPTIONS

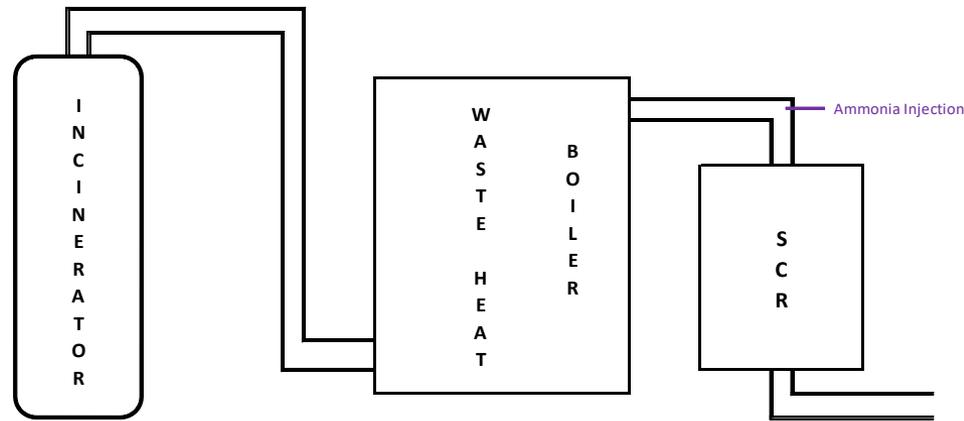


a) Traditional with Separate ESP & SCR

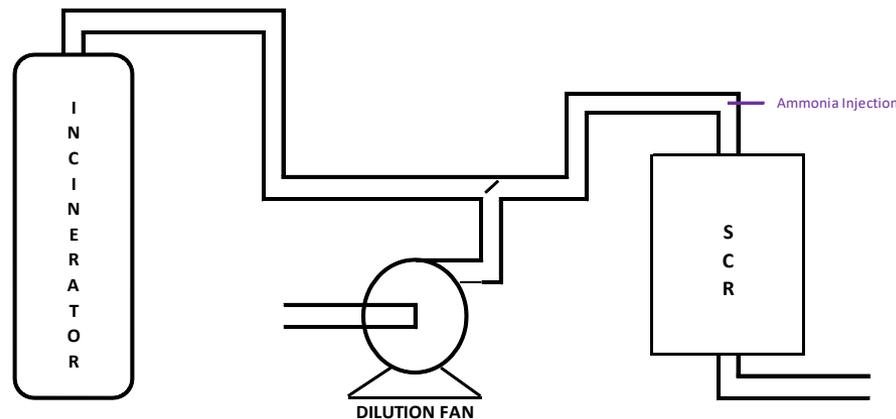


b) SCR Incorporated into ESP Using Catalytic Candle Filters

INCINERATOR NO_x CONTROL OPTIONS



a) Waste Heat Boiler



b) Dilution Air Fan

LOW NO_x BURNERS

When Firing Refinery Gas:

Low NO_x Burners ~ 30 – 40 ppm NO_x

Current Ultra Low NO_x Burners ~ 20 ppm NO_x

Next Generation Ultra Low NO_x Burners < 10 ppm NO_x

The Next Generation Ultra Low NO_x Burners Include the ClearSign Core Burner and John Zink Hamworthy's SOLEX Burner

Status

ClearSign

World Oil Testing Scheduled Week of November 16

Retrofit Scheduled for Q1 2021

John Zink Hamworthy

?

COST EVALUATION

Three Sources of Cost Estimates

- EPA SCR Cost model
- Unit-specific costs derived for refiners
- Western States Petroleum Association (WSPA) capital cost relationship

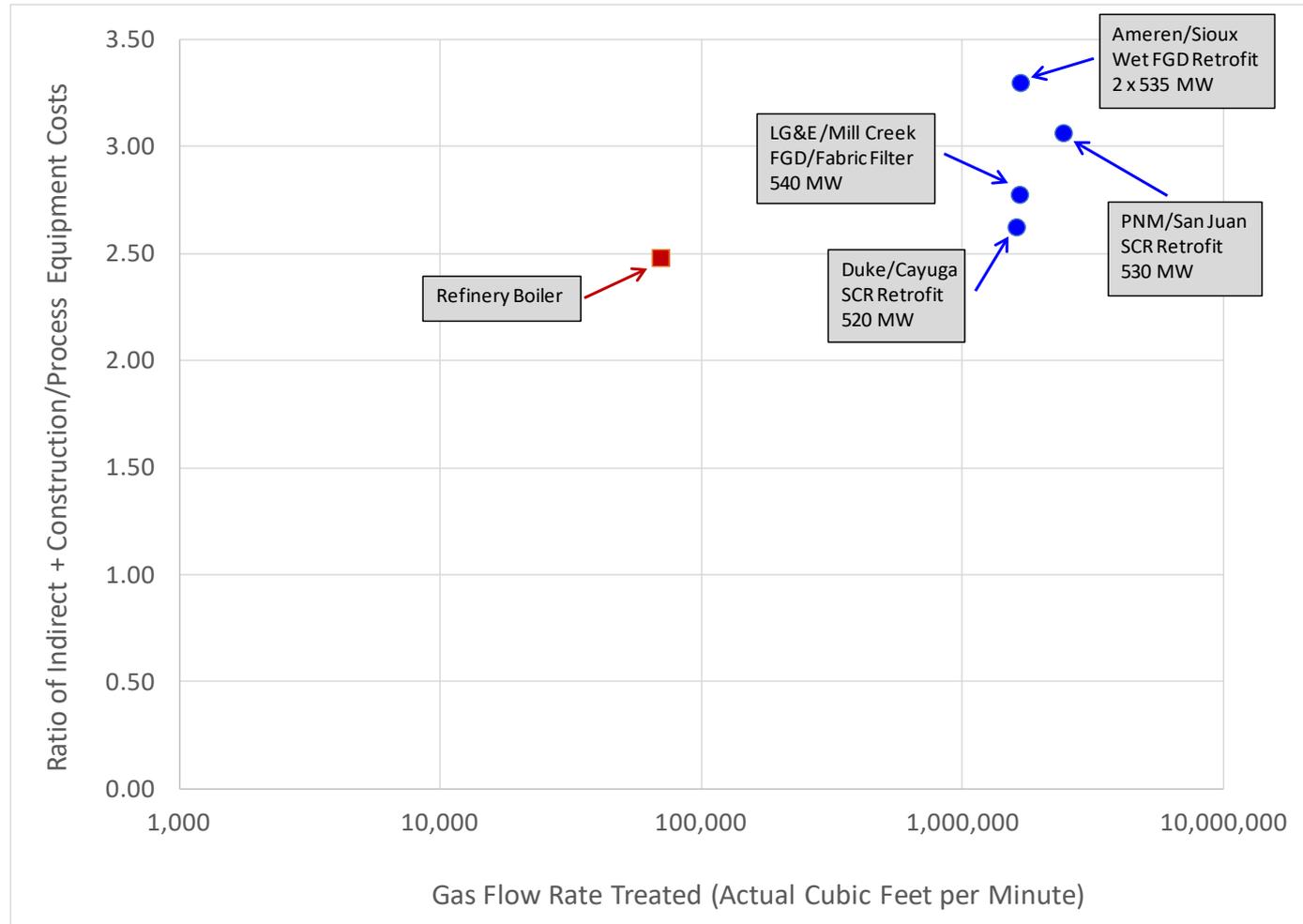
Revise EPA SCR Cost Model per Additional Inputs

- WSPA, refiner-specific data used to modify cost relationships
- Catalyst volume assignment, “refined” per additional data from catalyst suppliers
- Variable, fixed O&M costs adjusted to reflect refinery (not power generation) experience

INDIRECT/DIRECT COST RATIO

**Indirect Costs
2X-3X Direct
Costs**

**Broadly
Observed:
Electric
Generating
Units, Refinery
Applications**



Questions?

www.ferco.com

lmuzio@ferco.com

